

# Engineering Hierarchically Porous Carbon Using a Facile Process: Assessment for Green Electrodes

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**Abstract:** Production of carbonaceous materials from waste biomass is currently gaining much attention in scientific community due to the encouragement towards a sustainable approach. However, severe pretreatment processes are still the main challenging tasks. Herein, water hyacinth (WH) is used as a precursor. Hydrothermal carbonization in acidic conditions followed by thermal activation was used for the pretreatment. A novel chemical activator  $\text{CH}_3\text{COOK}$  was employed and compared to traditional chemical activators such as  $\text{ZnCl}_2$  and  $\text{K}_2\text{CO}_3$ . High surface areas and numerous micropores of synthesized carbons are found in  $\text{ZnCl}_2$  activation, while carbon compounds produced from  $\text{K}_2\text{CO}_3$  and  $\text{CH}_3\text{COOK}$  possess modest surface areas but hierarchically micro-meso-structured carbon. These findings demonstrate that the  $\text{CH}_3\text{COOK}$  could serve as both a reagent for acid-assisted hydrothermal carbonization and a doped chemical for thermal activation. The use of  $\text{CH}_3\text{COOK}$  is more ecologically and economically friendly, confirmed by reduced chemical usage and less produced wastewater. Furthermore, because the obtained carbons include a large number of nitrogen contents of around 2.0 wt%, these hierarchically porous carbons could enhance their performances as electrode materials in energy storage applications.

**Keywords:** Water hyacinth, Hydrothermal carbonization, Biomass conversion, Hierarchical porous carbon, Potassium acetate

## 1. Introduction

The growth of the world's population has caused an imbalance between the production and consumption of our feedstock, resulting in the lack of consistent access to enough food but somehow generating excessive garbage and polluting the environment [1]. Accordingly, alternative feedstock and sustainable management of the produced waste are crucial. Agricultural residues and food waste such as rice husk, corn hull, sugar cane straw, wheat straw, and coffee grinds are examples of biomass. Although there are several strategies to transform biomass into valuable products, including biodiesel, bio-coal, and alcohol, activated carbon manufacturing from these feedstocks has attracted a great deal of attention nowadays [2].

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Activated carbons derived from a sustainable resource have several positive aspects. The resultant carbons perform remarkably well enough in electrochemical investigations due to their highly porous architectures, which feasibly enable ion or charge transport [3]. Polar functional groups on the carbon matrix, such as hydroxyl, carbonyl, carboxylate, ether, and ketone, could enhance the wettability of polar electrolytes, allowing the passage of ions/charges [3]. Additionally, since heteroatoms such as phosphorous, nitrogen, and sulfur are naturally found in the feedstock as pigment compounds or amino acids, the self-doping of heteroatoms into carbon structures is more facile and eventually provides a substitute for conventional chemical doping [4,5]. Several investigations have been achieved in doping heteroatoms into carbon structures, significantly improving electrochemical performances by introducing pseudocapacitance into the materials [5,6]. Considerably, employing heteroatom-doped carbonaceous materials as a green electrode for energy storage devices, e.g., lithium-ion batteries and supercapacitors, is thus one of the most feasible strategies in biomass utilization.

Water hyacinth (*Eichhornia crassipes*, WH) is a notorious aquatic plant with an incredible growth rate over the water surfaces, resulting in the depletion of dissolved oxygen and nutrients and negatively impacting the ecosystem [7]. On the other hand, WH is predominantly composed of cellulose, hemicellulose, and lignin, but it also has a high protein content in its composition [7]. Such renewable resources can be utilized as a precursor for producing heteroatom-doped activated carbon.

Recently, we developed an approach for producing activated carbon from spent coffee grounds using hydrothermal carbonization (HTC) in an acetic acid solution, followed by potassium hydroxide (KOH) activation [6]. The findings demonstrate the significance of acidic conditions during HTC, which would be advantageous for introducing nitrogen atoms into carbon structures [6]. However, activation of hydrochar with base reagents tends to create a higher proportion of large mesopores and produce a very low carbon yielding. On the contrary, activation with acidic chemicals such as zinc chloride ( $ZnCl_2$ ) would enhance a larger degree of micropores in the carbon structures [8]. Although the existence of mesoporous features on carbon substrates would enhance electrolyte transport, the major of charge or ion transfer and storage is provided by the micropores [9]. Therefore, the production of carbon materials should be further optimized eventually for the hierarchical porous carbon. Rakmae and co-workers (2016) found that calcination can convert potassium acetate ( $CH_3COOK$ ) to carbonate species in the zeolite pores. The  $CH_3COOK$  precursor has the benefit of promoting a great dispersion of potassium carbonate ( $K_2CO_3$ ) on the zeolite support, resulting in superior catalytic performance for biodiesel production [10]. As a consequence, because  $CH_3COOK$  is an acidic medium that can be converted to basic  $K_2CO_3$  by thermal activation, such technique is adopted for the production of biomass-based carbon materials employing HTC pretreatment in an acidic environment followed by thermal activation.

Accordingly, this contribution highlights not only a straightforward but also an effective method for utilizing WH to produce carbon materials with high surface areas and nitrogen-containing in their structure. For the WH pretreatment, HTC and thermal activation were used.  $ZnCl_2$  and  $K_2CO_3$ , two typically chemical activators, were tested and compared with the novel chemical activator as potassium acetate  $CH_3COOK$ . Moreover, this study also presents preliminary results of those materials' electrochemical performances for use as green electrodes in supercapacitors. This established procedure is a potential strategy to be implemented in a practical application to facilitate activated carbon manufacturing and the SDGs in terms of converting waste into high-value goods.

## 2. Methodology

WH was collected from the Premprachakorn Canal in Pathum Thani, Thailand. In this study, the entire WH, including the stem, leaf, and root, was used as a sustainable resource for pretreatment. Afterward, WH was washed to eliminate dust, meshed, and dried. The WH was pretreated in an autoclave reactor using the hydrothermal method in 2 M acetic acid solution for 10 h at 180 °C. After the HTC process, WH-derived biochar was filtered, washed, and rinsed with DI water until the pH of the washing water was neutral. The biochar was then impregnated with chemical activators such as  $ZnCl_2$  and  $K_2CO_3$  in a 1:2 weight ratio of biochar : activator. Thermal activation was carried out in a tube furnace

for 2 h at 700 °C with N<sub>2</sub> gas flow (99.999%) at the flow rate of 350 mL·min<sup>-1</sup>. The resultant carbons were collected, rinsed with a large amount of DI water until the pH reached 7.0, and dried in a vacuum oven overnight at 50 °C.

All the preceding steps were replicated when CH<sub>3</sub>COOK was used as a chemical activator; however, the HTC was carried out in a 2 M acetic acid/potassium acetate solution (CH<sub>3</sub>COOH/CH<sub>3</sub>COOK). Additionally, subsequent filtering of as-prepared biochar, the biochar was subjected to thermal activation without any washing, pH adjusting, or chemical doping.

The elemental compositions of porous carbons were evaluated using an elemental analyzer (CHN62, LECO) and a sulfur analyzer for material characterization (628S, LECO). The porous architectures of the carbons were studied using N<sub>2</sub> adsorption-desorption analysis on an Autosorb IQ gas analyzer at -196 °C, and the materials had to be degassed for 3 h under a vacuum before analysis. The specific surface areas, pore size distribution and microporous surface area, and pore volume were calculated using the Brunauer-Emmett-Teller (BET), the Non-Localized Density Functional Theory (NLDFT) and t-plot methods, respectively. The surface morphology of carbons was examined by the scanning electron microscope (SEM) on a Hitachi SU8030. The topology of the carbon microstructure was obtained using a transmission electron microscope (TEM) on a JEOL TEM-2100. Carbon allotropes were determined using an X-ray diffractometer (XRD) on a Bruker D8 Advance with Cu K $\alpha$  radiation (1.54 Å) operated at 40 kV and 40 mA, scanning in the range of 2-theta (2 $\theta$ ) between 10° and 80° at a rate of 0.02° min<sup>-1</sup> and step time 0.5 s·degree<sup>-1</sup>. Characteristics of carbons were examined using the Raman spectrometer on NT-MDT NTEGRA at the excitation wavelength ( $\lambda_{ex}$ ) of 532 nm.

The electrochemical properties of porous carbons were investigated using a potentiostat (Metrohm Autolab) equipped with a three-electrode system, including Ag/AgCl, Pt wire, and synthesized carbons as reference, counter, and working electrodes, respectively. Working electrodes were fabricated by sputtering the slurry containing 80 activated carbons : 10 carbon black : 10 polyvinylidene fluoride (PVDF) mass ratio on the 316 stainless steel sheets with a confined area of 1 cm<sup>2</sup>. Prior to usage, the working electrodes were dried for 12 h at 60 °C in a vacuum oven. Cyclic voltammetry (CV) and galvanostatic charge/discharge (GCD) were conducted in 1 M H<sub>2</sub>SO<sub>4</sub> as an electrolyte with varied scan rates and current densities. Specific capacitance (C<sub>s</sub>) values were calculated by the following Equation 1:

$$C_s = \frac{I \cdot \Delta t}{m \cdot \Delta V} \quad (1)$$

Where  $I$  is constant discharge current (A),  $\Delta t$  is discharge time (s),  $m$  is mass of active materials (g), and  $\Delta V$  is discharge potential range (V).

### 3. Results and discussion

#### Effect of chemical activators on physical properties of activated carbons

AC-1, AC-2, and AC-3 signify activated carbons produced through ZnCl<sub>2</sub>, K<sub>2</sub>CO<sub>3</sub>, and CH<sub>3</sub>COOK activation, respectively. Total utilization of the WH for the sustainable production of porous carbons was successfully investigated, demonstrating a high yield of carbon products of up to 20%. Table 1 shows the elemental compositions of carbon samples. AC-1 demonstrates carbon as a major component, but AC-2 and AC-3 show both carbon and oxygen as substantial components. The presence of oxygenated species in the carbon structure may enhance the hydrophilicity of such an activated carbon for its functions [3]. Interestingly, following the pretreatment process, the results show that nitrogen levels of almost 2.0 wt% are retained in carbon structures. Indeed, nitrogen content in the carbon structure can promote not only hydrophilicity but also pseudocapacitance for electric double-layer supercapacitors (EDLC), which can further improve electrode performance [6]. Nevertheless, non-specified elements of around 20-30% in the prepared activated carbon must be further examined.

The XRD pattern of the obtained materials (Figure 1(a)) reveals a broad peak at 2 $\theta$  of about 23.0°, corresponding to amorphous graphitic carbon [11]. In contrast, sharp peaks at 2 $\theta$  of 21.0° and 26.0° in the AC-1 are assigned to quartz which might be attributed to the re-crystallization of silica in the WH structure during calcination

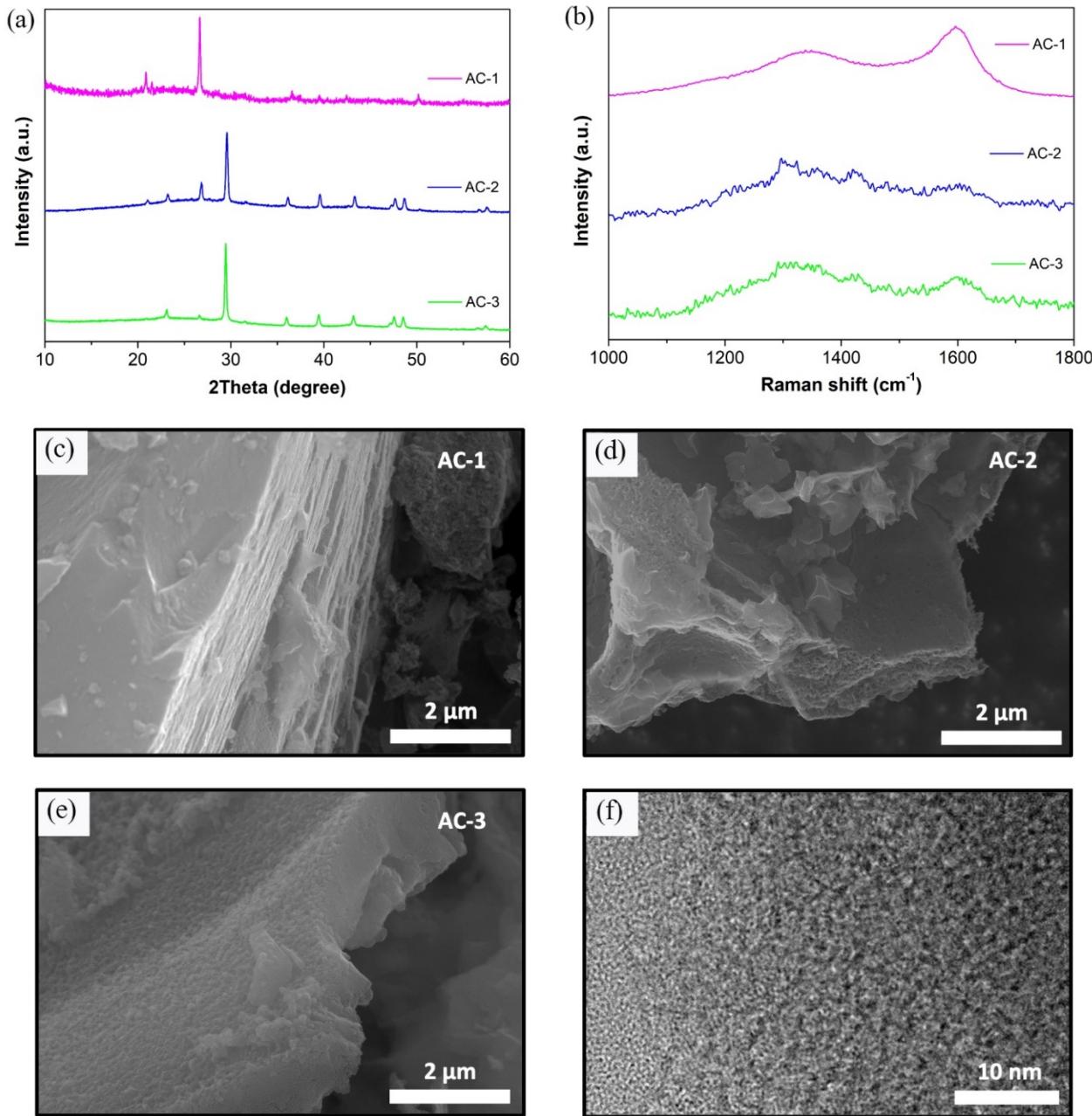
[12]. Indeed, amorphous carbon and composite silica/carbon structures can improve the performance of energy storage devices, particularly lithium-ion batteries during the lithiation and delithiation processes [13]. Moreover, dominant peaks at  $2\theta$  of  $23.0^\circ$ ,  $29.5^\circ$ ,  $36.0^\circ$ ,  $39.5^\circ$ ,  $43.1^\circ$ ,  $47.8^\circ$  and  $48.7^\circ$  in the AC-2 and AC-3 are interpreted as calcite presenting in ash after thermal activation [14,15]. These noticeable minerals in the XRD results are consistent with a large number of unspecified elements observed in the elemental analysis. The Raman spectra of the resultant carbons in Figure 1(b) illustrate the distinctive peaks about  $1350$  and  $1590\text{ cm}^{-1}$  corresponding to the D- and G-bands of disordered and ordered carbon structures, respectively. Additionally, the D-band to G-band ( $I_D/I_G$ ) ratio can be used to determine the degree of graphitization, with a lower  $I_D/I_G$  ratio indicating that the carbon materials are highly graphitized [16]. The  $I_D/I_G$  ratio of the AC-1 is  $0.90$ , while this value increases to  $\sim 1.06$  for the AC-2 and AC-3, indicating a well-developed graphitic carbon structure of the AC-1 that might enhance the electrical conductivity of activated carbons [11]. The SEM image in Figure 1(c) shows a well-developed stacked sheet structure of AC-1 with small attached carbon particles. In contrast, a very rough external surface and non-uniform carbon structure are observed in AC-2 and AC-3 (Figure 1(d-e)). The TEM image of the AC-1 in Figure 1(f) indicates dispersed worm-like micropores in the amorphous carbon matrix.

**Table 1** Elemental compositions of carbon samples obtained by the CHNS analyzer

Samples	Elements (wt%)					
	C	N	O	S	H	Others
AC-1	64.27	2.51	11.03	0.33	1.51	20.35
AC-2	39.98	1.19	22.99	0.13	2.61	34.11
AC-3	37.40	1.88	25.12	0.36	2.59	32.74

Another significant property that should be considered is the textural properties since they strongly impact the transportation of ions and charge in the electrodes [17]. Figure 2(a) shows  $N_2$  adsorption/desorption isotherms of AC-1, AC-2, and AC-3 as well as their pore size distribution histogram; in addition, the information including specific surface area ( $S_{BET}$ ), microporous surface area ( $S_{mic}$ ), total pore volume ( $V_{total}$ ) and average pore diameter ( $D_{aver}$ ) is summarized in Table 2. All samples exhibit a major characteristic of type I isotherm, revealing high  $N_2$  uptake at low  $P/P_0$ . However, a hysteresis loop at high  $P/P_0$  can be related to type IV isotherm, demonstrating mesoporous structures. Accordingly, these results imply the formation of hierarchically porous structures of the obtained carbons. Their hierarchical porous structures can be also confirmed by the pore size distribution (Figure 2(b)), clarifying the distribution of pore diameter significantly at around  $1.0\text{ nm}$  and partially between  $2\text{-}10\text{ nm}$ . Interestingly, the  $S_{BET}$  of AC-1 ( $1353\text{ m}^2\cdot\text{g}^{-1}$ ) is around 2.6 folds higher than that of the  $S_{BET}$  of AC-2 ( $535\text{ m}^2\cdot\text{g}^{-1}$ ) and AC-3 ( $511\text{ m}^2\cdot\text{g}^{-1}$ ), while the degree of  $S_{mic}$  of 80% is prominent in AC-1 and AC-3, compared to 64% in AC-2. A higher proportion of micropores in porous carbons derived from acidic activators (AC-1 and AC-3) with respect to base activator (AC-2) can be explained by the fact that acidic activation has a low carbon content degradation rate than base activation because of the differences in the activation mode [18,19], resulting in a higher degree of micropores rather than a higher fraction of larger pores. As  $ZnCl_2$  can serve as a template in the dehydration process for the formation of porosity in confined spaces inside precursor particles, the small and uniform size of the micropores is created. However,  $K_2CO_3$  activation is typically accomplished by a redox process. The reduced metallic potassium is intercalated inside the graphitic laminar structure. Carbon is oxidized to  $CO$  or  $CO_2$ , and the solid particle degrades, resulting in a higher proportion of mesoporosity, mainly at the outermost surfaces of carbon materials [19]. The explanation is also consistent with the results of SEM images, which reveal that the external surfaces of AC-2 and AC-3 are rougher than AC-1. Therefore, the results from  $N_2$  adsorption/desorption demonstrate beneficial aspects for the use of  $CH_3COOK$  as a chemical activator by enhancing the degradation rate of carbon contents but lowering the formation of mesoporosity. It should be noted that a large specific surface area accompanied by a predominance of micropores may promote sufficient ion or charge accumulating areas on the electrode/electrolyte interface, whereas the coexistence of larger mesopores may provide

a more facile electrolyte transport, further improving the charge/ion transference capability [17]. As a result, activated carbon with hierarchically micro/mesoporous structures is advantageous for high-performance energy storage electrodes.



**Figure 1** Characterization of carbon materials: (a) XRD patterns, (b) Raman spectra, (c), (d), (e) SEM images of the AC-1, AC-2 and AC-3, respectively, and (f) TEM image of the AC-1.

All things considered, the use of  $\text{CH}_3\text{COOK}$  as a chemical activator for WH pretreatment has several significant advantages, including no more added chemical doping during the thermal activation process, less produced wastewater during filtration and neutralization, and self-doped N contents in a hierarchically porous carbon matrix. Nevertheless, modest specific surface areas and a significant number of inorganic components in carbon frameworks, which would dramatically alter carbon's conductivity, are bottlenecks that should be further improved.

Table 2 Summarized information on textural properties of carbon samples

Samples	$S_{\text{BET}}^a$ ( $\text{m}^2 \cdot \text{g}^{-1}$ )	$S_{\text{mic}}^b$ ( $\text{m}^2 \cdot \text{g}^{-1}$ )	% $S_{\text{mic}}$	$V_{\text{total}}^c$ ( $\text{cm}^3 \cdot \text{g}^{-1}$ )	$D_{\text{aver}}^c$ (nm)
AC-1	1353	1076	79.5	0.81	1.27
AC-2	535	341	63.7	0.48	1.06
AC-3	511	409	80.0	0.36	1.06

Remarks: <sup>a</sup>  $S_{\text{BET}}$  was calculated from the Brunauer-Emmett-Teller (BET).

<sup>b</sup>  $S_{\text{mic}}$  was adopted from the Non-Localized Density Functional Theory (NLDFT).

<sup>c</sup>  $V_{\text{total}}$  and  $D_{\text{aver}}$  were derived from the t-plot method.

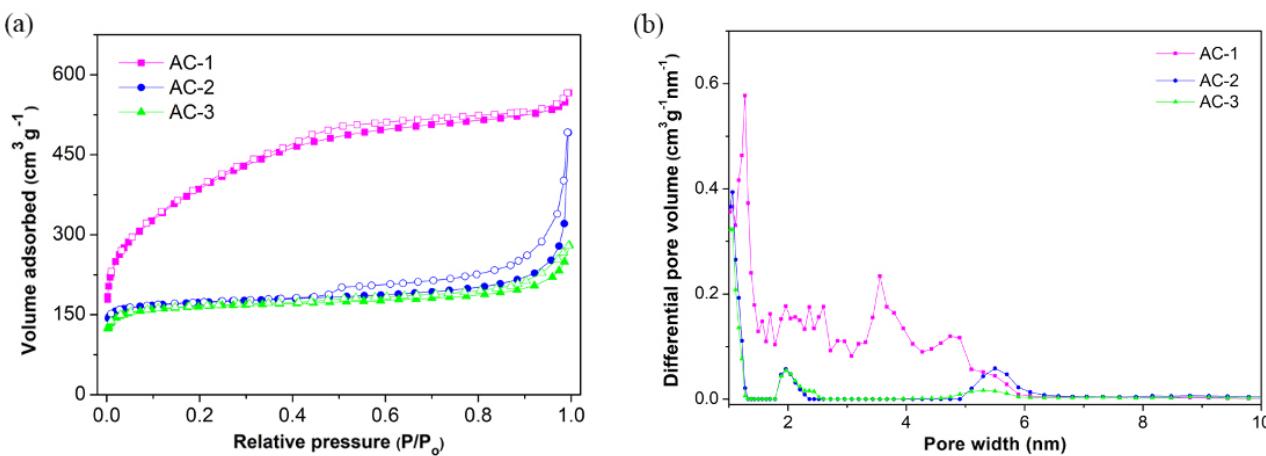
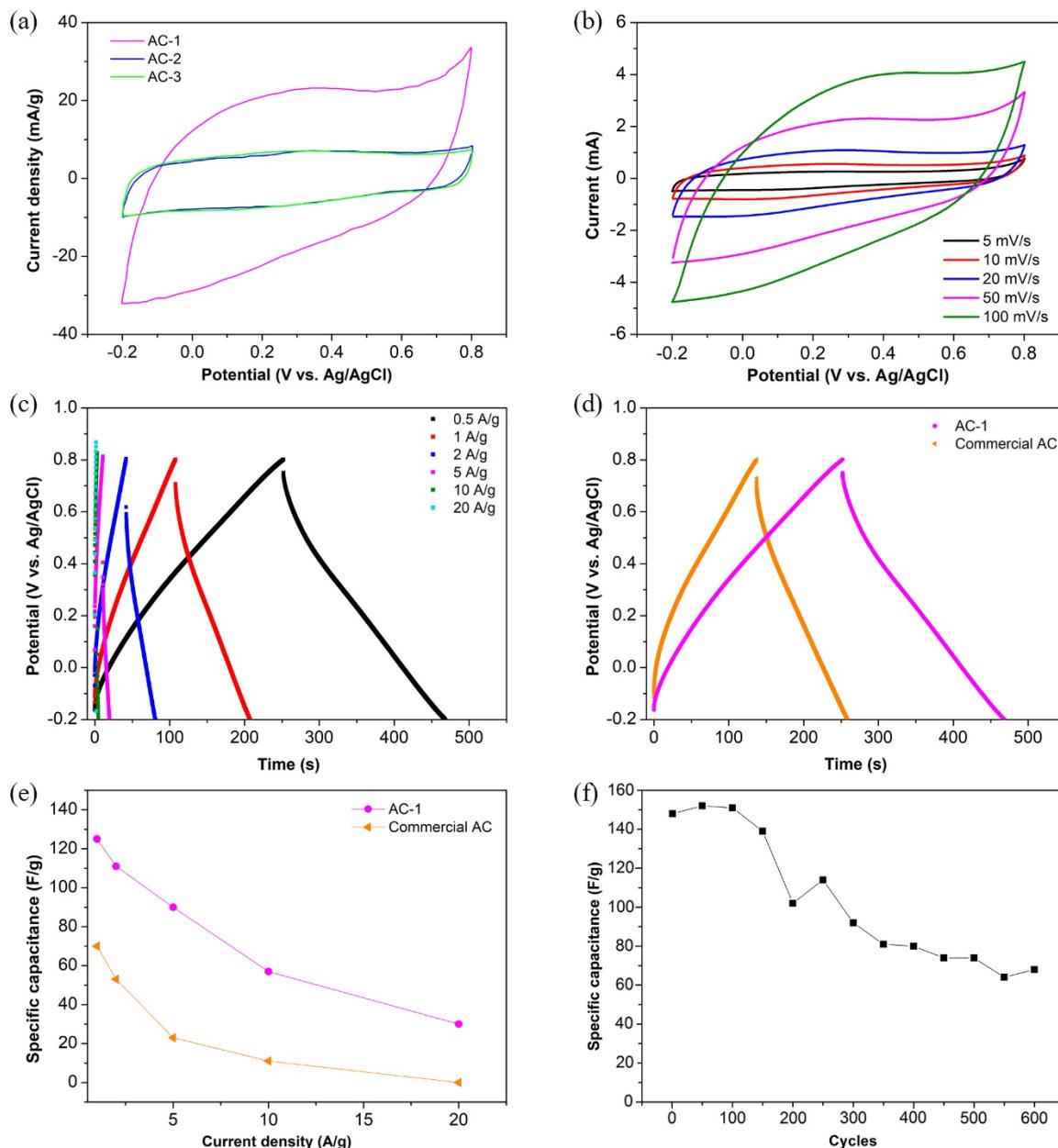


Figure 2 Textural properties of carbon samples: (a) N<sub>2</sub> adsorption/desorption isotherm and (b) pore size distribution histogram of AC-1 (pink), AC-2 (blue), and AC-3 (green). In cases of the N<sub>2</sub> adsorption/desorption isotherm, solid and space symbols represent adsorption and desorption regions, respectively.

### Electrochemical performances of activated carbons

The produced activated carbons were initially used as a green electrode for a supercapacitor. All electrochemical performances were tested in a three-electrode system in 1 M H<sub>2</sub>SO<sub>4</sub> as an electrolyte solution. The CV curves of all samples at a scan rate of 50 mV/s are displayed in Figure 3(a). These materials exhibit quasi-rectangular CV curves, indicating efficiently reversible supercapacitor behavior [20]. Interestingly, the larger area of the AC-1 than that of the others demonstrates its greater charge accumulating capability due to its large specific surface areas and significant N contents [21]. Consequently, AC-1 was chosen for further studies. The CV curves of the AC-1 at different scan rates shown in Figure 3(b) still maintain a distorted rectangular-like shape, implying a good EDLC paired with pseudocapacitive performance [22]. In reality, EDLC behavior results from ion or charge storage at the electrode/electrolyte interfaces, whereas pseudocapacitive performance originates from redox reactions between heteroatom moieties and ions in the electrolyte [22]. The similar shapes of CV curves at both low and high scan rates indicate that ions or charges can effectively excess into electrode surfaces [22]. Figure 3(c) shows nearly symmetric and linear GCD curves at various current densities, along with a slight distortion and a small IR drop at high current density (0.05 V at 0.5 A·g<sup>-1</sup>), confirming reversible charging/discharging and demonstrating the behavior of the EDLC coupling with pseudocapacitance reaction [22]. Furthermore, the quasi-triangle GCD curve of the AC-1 compared to the relatively symmetric GCD curve of the commercial AC demonstrates the evident pseudocapacitance of the obtained material in the H<sub>2</sub>SO<sub>4</sub> electrolyte (Figure 3(d)). The specific capacitance (C<sub>s</sub>) of electrodes at different current densities was determined and reported in Figure 3(e). The AC-1 reaches a significant C<sub>s</sub> value of 125 F·g<sup>-1</sup> at 1 A·g<sup>-1</sup>, while the commercial AC only possesses a value of 70 F·g<sup>-1</sup>, indicating a quite competitive capability as electrode materials for

supercapacitors.  $C_s$  values dramatically decline as the current density increases (Figure 3(e)). The decrease in  $C_s$  can be explained by insufficient path length of ions or charges in the electrolyte to transport into the electrode interfaces [23]. The cycling stability of the AC-1 was tested, as shown in Figure 3(f). The significant reduction of the  $C_s$  values can be found at approximately 50% after 500 times charge-discharge cycles at  $1 \text{ A}\cdot\text{g}^{-1}$ , revealing moderate capacitance retention and cycle performance. For the practical application of the synthesized material in a supercapacitor, other electrochemical tests have to be further explored such as the Electrochemical Impedance Spectroscopy (EIS), investigating in a symmetric two-electrode system or eventually symmetric coin-type supercapacitor devices.



**Figure 3** Electrochemical performance of activated carbons: (a) CV curves of the AC-1, AC-2, and AC-3 at a scan rate of 50 mV/s, (b) CV curves of the AC-1 at varied scan rates, (c) GCD curves of the AC-1 at different current densities, (d) GCD curves of the AC-1 compared to a commercial AC at a current density of 0.5 A/g, (e) specific capacitance versus current density of the AC-1 compared to a commercial AC, and (f) retention performance of the AC-1. Electrochemical characterization was conducted in a three-electrode system in 1 M  $\text{H}_2\text{SO}_4$  as an electrolyte solution.

## 4. Conclusion

In summary, hydrothermal carbonization followed by thermal activation was applied to produce activated carbons derived from WH. A novel chemical activator  $\text{CH}_3\text{COOK}$  was applied for the pretreatment process compared to conventional  $\text{ZnCl}_2$  and  $\text{K}_2\text{CO}_3$  activators.  $\text{CH}_3\text{COOK}$  can act, at the same time, as a reagent for acid-assisted hydrothermal carbonization to enhance carbon yield and as a doped chemical for thermal activation to create porosity. Activated carbons derived from  $\text{CH}_3\text{COOK}$  possess a moderate surface area of around  $500 \text{ m}^2\cdot\text{g}^{-1}$  and show hierarchically micro/mesoporous structures. The developed pretreatment process is greener and more cost-effective than the general two-step pretreatment procedure. However, the structural, topological, and electrochemical properties of activated carbons should be closely monitored. The AC-1 has large surface areas and considerable nitrogen contents in its carbon backbone. Consequently, the AC-1 exhibits EDLC and pseudocapacitive characteristics of specific capacitance of  $125 \text{ F}\cdot\text{g}^{-1}$  at  $1 \text{ A}\cdot\text{g}^{-1}$ , which are beneficial for energy storage devices and could be used as electrode materials for supercapacitors.

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