

# M<sup>2+</sup>(Ni, Cu, Zn)/Al-LDH Composites with Hydrochar from Rambutan Peel and Study the Adsorption Efficiency for Organic Dyes

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## ABSTRACT

Ni/Al LDH, Cu/Al LDH, and Zn/Al LDH were composed with rambutan peel hydrochar (Hc) and the materials were applied as adsorbent for the removal of methylene blue from aqueous solution, measured using UV-Vis Spectrophotometric method. The preparation of the LDH-Hc composites were proven by XRD, FT-IR, and SEM analysis which showed similar characteristics of the LDH-Hc composites with pure LDH and hydrochar. The methylene blue removal efficiency was optimized by various parameters including adsorption selectivity, adsorption regeneration, pH, contact time, adsorption concentration, and temperature. The adsorption study analysis proved that LDH composited with rambutan peel hydrochar had a selective ability for methylene blue. Zn/Al-hydrochar had the most stable adsorption regeneration ability and adsorbed MB easily after seven regeneration cycles using water solvents and ultrasonic devices. Ni/Al-hydrochar and Cu/Al-hydrochar were effective up to five regeneration cycles for MB removal. The adsorption results showed that the optimal pH for MB adsorption was at pH 6 with an equilibrium adsorption contact time of 100 min and a tendency to follow the pseudo second order kinetic model. Parameter data of concentration and temperature of adsorption was determined using Langmuir and Freundlich equations. The results showed that the adsorption matched the Freundlich isotherm model with the adsorption capacity ( $q_m$ ) of Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc adsorbents reaching 144.928, 175.439, 217.391 mg/g, respectively, with the adsorption process taking place continuously, spontaneously, and endothermically.

## 1. INTRODUCTION

Methylene blue (MB) is the most widely used dye in industry (Xu et al., 2020) such as pharmaceutical, paper, textile, paint, and plastic industries (Ahmad et al., 2020; Dang et al., 2020; Mantasha et al., 2020; Wang et al., 2016). Dyestuff waste is one of the environmental pollution problems that must be overcome to ensure sustainable industrial production (Nakhli et al., 2020). Methylene blue is a cationic dye that is classified as a toxic dye with mutagenic and carcinogenic properties that will significantly affect human health which can cause neuronal apoptosis, increased heart rate, inflammation of the leptomeninges, nausea, and vomiting and harm

aquatic ecosystems (Alver et al., 2020; Liao et al., 2020; Nakhli et al., 2020).

Therefore, industrial waste treatment needs to be carried out to reduce the concentration of waste before being discharged into the environment. To overcome pollution in wastewater, various methods can be used such as adsorption, photocatalytic separation (Karagöz et al., 2008), membrane processes, coagulation, biodegradation (Li et al., 2020a), flocculation (Li et al., 2020b), aerobic and anaerobic treatment, ion exchange and electrochemistry (Ebadollahzadeh and Zabihi, 2020). Among them, the simplest, cheapest, and most effective wastewater treatment process is adsorption

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(Badri et al., 2020), one of the main industrial wastewater treatment methods for effluent purification. Adsorption is a method of transferring pollutant molecules to solid materials that can selectively remove pollutants from liquid waste by attracting pollutant molecules to the surface of the adsorbent (Alver et al., 2020). However, to reduce processing costs, efforts can be made to use alternative adsorbents that are cheap, abundant and easy to find. Recently, many studies have developed inexpensive and effective adsorbents to remove dyes in industrial waste made from agricultural wastes (Alinezhad et al., 2020). In the literature, a number of adsorbents have been investigated such as clay (Adeyemo et al., 2017), duku peel (Juleanti et al., 2021), wood waste (Stjepanović et al., 2021), orange peel (Chopra et al., 2012), plant biomass (Yeow et al., 2021), pineapple (Mahmuda et al., 2021), rice husk (Palapa et al., 2020a), coconut husk, bamboo dust (Rafatullah et al., 2010), and rambutan peel (Normah et al., 2021a).

Rambutan peel has been reported to have main chemical components containing cellulose, lignin, hemicellulose and phenolic compounds. This research conducted by Castro and das Virgens (2019) supports the effective application of rambutan skin as an adsorbent. Some of the advantages of rambutan peel as an adsorbent include having a good adsorption capacity, selective adsorption and can be regenerated (Mahmuda et al., 2021; Alrozi et al., 2012; Setiawan et al., 2018). Therefore, the conversion of rambutan peel into an adsorbent will provide an alternative that has the potential to be modified with layered double hydroxide to form a composite.

Layered double hydroxide or LDH is an anionic clay material that has a two-dimensional (2D) structure and contains anions in the interlayer, LDH is the same as hydrotalcite which is composed of divalent ( $M^{2+}$ ) and trivalent ( $M^{3+}$ ) metals which have the general formula  $[M^{2+}_{1-x}M^{3+}_x(OH)_2] [A^{n-}_{x/n}] \cdot mH_2O$ ,  $A^{n-}$ : interlayer anions as charge balance (Lu et al., 2020; Xu et al., 2021). LDH has the advantage of producing a material that has a large adsorption capacity and is flexible (Lesbani et al., 2020; Normah et al., 2021b). However, LDH cannot be recycled and cannot be used in a regeneration process. Therefore, a method is needed to produce a stronger structure so that it can be used repeatedly by being composited with a supporting material (Wijaya et al., 2021).

Based on several investigations, LDH can be composited with biochar, zeolite, graphite, and chitosan (Bezerra et al., 2021; Fang et al., 2021).

Zubair et al. (2018) reported that Ni/Fe LDH was composited with starch and applied to remove methyl orange in the liquid phase with a maximum adsorption capacity of 387.59 mg/g and a stable regeneration cycle reaching four cycles for the starch composite adsorbent NiFe-LDH. Alagha et al. (2020) reported Mg-Fe/LDH magnetic composite with activated carbon was applied to remove nitrate and phosphate in wastewater with reusability performance results with five regeneration cycles.

This study aimed to modify the LDH in the form of Ni/Al, Cu/Al, and Zn/Al composites with hydrochar rambutan peel, characterized using XRD, FT-IR, and SEM analysis. The adsorbent was applied for the selectivity of organic dyes in the form of methylene blue (MB), Rhodamine-B (Rh-B), methyl orange (MO), methyl red (MR), then the adsorbent would be tested for effectiveness in studies of regeneration, adsorption isotherms, and adsorption thermodynamics with the most selective dyes with adsorbents.

## 2. METHODOLOGY

### 2.1 Materials

The chemicals used to synthesize materials are nickel(II) nitrate ( $Ni(NO_3)_2 \cdot 3H_2O$ , 99% purity) by Sigma Aldrich, copper(II) nitrate ( $Cu(NO_3)_2 \cdot 3H_2O$ , 98% purity) by LOBA Chemie, zinc(II) nitrate ( $Zn(NO_3)_2 \cdot 3H_2O$ , 98.9% purity) by Merck, aluminum(III) nitrate, ( $Al(NO_3)_3 \cdot 9H_2O$ , MW=375.13 g/mol, 98% purity) by Sigma Aldrich, hydrochloric acid (HCl, MW=36.458 g/mol, 37%), sodium hydroxide (NaOH, MW=40.00 g/mol by Merck, and the basic ingredient for making hydrochar is rambutan peel. Adsorbate used dye methylene blue (MB), Rhodamine-B (Rh-B), methyl orange (MO), and methyl red (MR).

### 2.2 Methods

#### 2.2.1 Rambutan peel preparation

Rambutan peel powder was prepared using rambutan peel that had been cleaned and then dried in the sun. The dried rambutan peel was cut into small pieces and then baked at 110°C for 8 h. Then, the peel was mashed and passed through a 50 mesh sieve.

#### 2.2.2 Hydrochar (Hc) preparation

Hydrochar was prepared using the hydrothermal carbonization (HTC) method (Li et al., 2020c) using a stainless steel autoclave hydrothermal device with 2.5 g of rambutan peel powder and 50 mL of distilled water tightly closed in the oven at 200°C

for 10 h. In the final process, the autoclave was cooled to room temperature and the product in the autoclave was filtered. The resulting solid (hydrochar) was dried at a temperature of 105°C. Hydrochar was analyzed by characterization with XRD, FT-IR, and SEM.

### 2.2.3 Composite LDH-Hc preparation

The preparation of LDHs into LDH-Hc composites was carried out by the coprecipitation method by preparing 30 mL of a solution of  $M^{2+}$  (Ni, Cu, and Zn) (0.75 M) mixed with 30 mL (0.25 M) aluminum (III) nitrate and stirred. A 2 M NaOH solution was added dropwise to the mixture until it reached pH 10 and was maintained for 1 h until a precipitate was formed. To the LDH-Hc composite precipitate mixture was added as much as 3 g of hydrochar powder from rambutan peel, then stirred and kept at 80°C for 72 h. The product from the process was filtered using a vacuum and rinsed with distilled water, and the resulting product was then dried at 60°C to dryness. The preparation results in the form of Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc were analyzed by XRD, FT-IR, and SEM.

### 2.2.4 Adsorption experiment procedure

Adsorption selectivity is done by mixing several dyes using the same concentration and the same volume of dye. The dyes were methylene blue (MB), rhodamine-B (Rh-B), methyl orange (MO), and methyl red (MR) with a concentration of 8 mg/L each of 50 mL, then the mixture was added to 0.05 g (rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc) and stirred using a shaker with time variations of 0, 15, 30, 60, to 120 min. After the expiration of each time, the mixture is separated by centrifugation to obtain the filtrate and residue, the filtrate is then analyzed for wavelength using a UV-Vis spectrophotometer in the range of 400-700 nm.

After obtaining the most selective dye, methylene blue (MB), adsorption studies using MB were done on each adsorbent.

The adsorption process of MB was studied through the influence of adsorption time. Various of the adsorption times were carried out with the concentration of MB 60 mg/L, then 20 mL was taken and added as much as 0.02 g of adsorbent and stirred for 0-150 min.

The kinetics adsorption was calculated using kinetic adsorption model such as pseudo first-order (PFO) and pseudo second-order (PSO). The formula should be written by:

$$\text{Pseudo first-order (PFO): } \log (q_e - q_t) = \log q_e - \left( \frac{k_1}{2.303} \right) t \quad (1)$$

$$\text{Pseudo first-order (PFO): } \frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \quad (2)$$

Where;  $q_e$  is adsorption capacity at equilibrium (mg/g);  $q_t$  is adsorption capacity at  $t$  (mg/g);  $t$  is adsorption time (min);  $k_1$  is adsorption kinetic rate at pseudo first-order (/min);  $k_2$  is adsorption kinetic rate at pseudo second-order (g/mg/min).

The adsorption isotherm model in the form of Langmuir and Freundlich models was used to determine the equilibrium adsorption capacity data and analyze the adsorption mechanism.

Langmuir and Freundlich isotherm equations are as follows:

$$\text{Langmuir: } \frac{C}{m} = \frac{1}{bK} + \frac{C}{b} \frac{C}{m} = \frac{1}{bK_{ML}} + \frac{C}{b} \quad (3)$$

Where;  $C$  is a saturated concentration of adsorbate;  $m$  is the amount of adsorbate;  $b$  is the maximum adsorption capacity (mg/g);  $K_{ML}$  is the Langmuir constant (mg/L).

$$\text{Freundlich: } \log q_e = \log K_F + \frac{1}{n} \log C \quad (4)$$

Where;  $q_e$  is adsorption capacity at equilibrium (mg/g);  $C_e$  is a concentration of adsorbate at equilibrium (mg/L);  $K_F$  is Freundlich constant.

The experimental adsorption isotherm was carried out with various initial concentrations of methylene blue (MB) (60, 70, 80, 90, and 100 mg/L) As much as 20 mL of MB solution was added to 0.02 g of adsorbent (rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc and Zn/Al-Hc) and stirred for 2 h with temperature variations of 30, 40, 50, and 60°C. The last process was the separation of solutions and solids using centrifugation, then the solution was measured using a UV-Vis Spectrophotometer.

Adsorption thermodynamics used to calculate the Gibbs free energy change data ( $\Delta G$ ), enthalpy ( $\Delta H$ ), and entropy ( $\Delta S$ ) calculated by Equation (5-6):

$$\Delta G = -RT \ln (K_d) \quad (5)$$

$$\ln K_d = \frac{\Delta S}{R} - \frac{\Delta H}{RT} \quad (6)$$

$K_d$  is the solute distribution coefficient (L/g);  $R$  is the universal gas constant (8.314 mol/K);  $T$  is

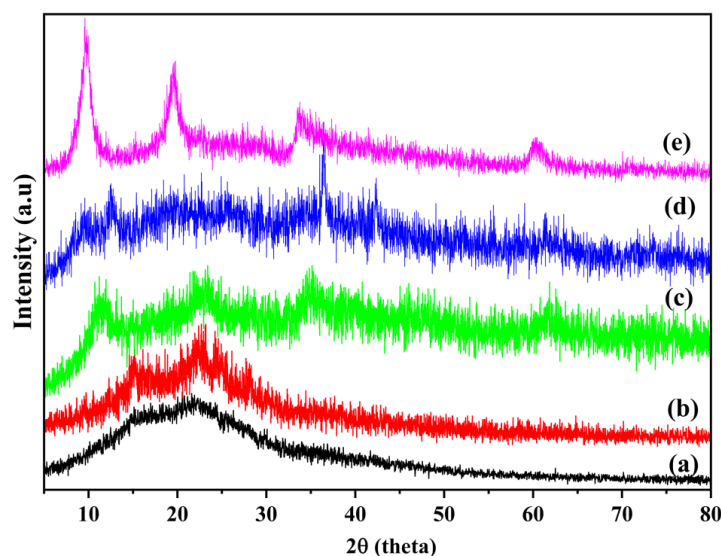
temperature (K); Gibbs free energy ( $\Delta G$ , kJ/mol); entropy ( $\Delta S$ , kJ/mol); and enthalpy ( $\Delta H$ , J/mol/K).

The regeneration process was carried out to test the effectiveness of the adsorbent in reusing the adsorbent. In this study, the regeneration process was carried out by adding 50 mL of adsorbate solution and 0.5 g of adsorbent (rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc). The mixture of adsorbent and adsorbate was stirred for 3 h then separated between the solution and residual adsorbent, the solution was taken and measured using a UV-Vis spectrophotometer, while the remaining adsorbent was dried at 40°C and reused through the desorption process. The desorption process was carried out by adding 50 mL of water to the residual adsorbent and then desorption using an ultrasonic device for 2 h. The adsorbent that has gone through the desorption process is dried and then reused for the next adsorption process for seven repetitions of the same procedure.

### 3. RESULTS AND DISCUSSION

The successful preparation of LDH-Hc composite materials in the form of Ni/Al-Hc, Cu/Al-

Hc, and Zn/Al-Hc was proven by the results of XRD, FT-IR, and SEM characterization analysis. The data characterization results are shown in Figure 1. Figure 1(a) shows an XRD diffractogram of rambutan peel with the appearance of two distinctive peaks at diffraction angles of 16° and 23.3° which describe that the rambutan peel contains cellulose compounds (Oliveira et al., 2016). Figure 1(b) shows the diffractogram of Hc material from the preparation of rambutan peel through the hydrothermal carbonization (HTC) process and shows a diffraction pattern similar to Figure 1(a). In the Hc diffractogram there was an increase in crystallinity, this was due to changes in amorphous cellulose compounds. The results of XRD characterization of composite materials were confirmed through the JCPDS (Joint Committee on Powder Diffraction Standard) data corresponding to each LDH. Typical diffraction peaks of Ni/Al LDH according to JCPDS data No.15-0087 (Wang et al., 2018), Cu/Al LDH with JCPDS No. 30-0630 (Palapa et al., 2020b) and Zn/Al LDH with JCPDS No. 48.2023 (Shin et al., 2020). The diffraction patterns of the Mg/Al-Hc, Ca/Al-Hc, and Zn/Al-Hc composites are presented in Figure 1.



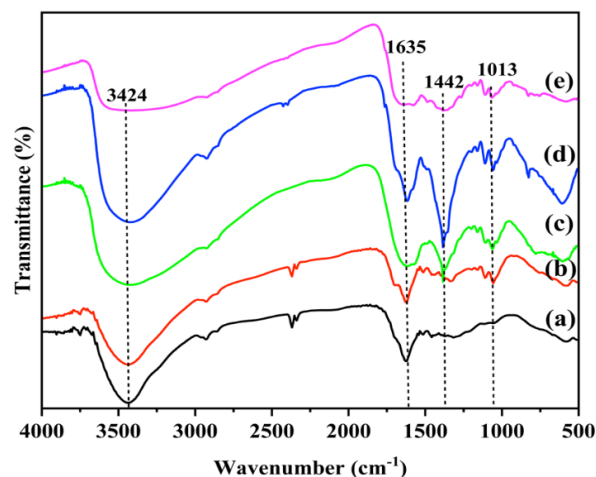
**Figure 1.** X-ray Powder diffraction patterns of rambutan peel (a), Hc (b), Ni/Al-Hc (c), Cu/Al-Hc (d), and Zn/Al-Hc (e)

Based on Figure 1, the diffraction peaks in Figure 1(c) which show the Ni/Al-Hc diffractogram at 2  $\theta$  angles 11.38°(003), 22.9°(002), 35.2°(012), 61.6°(110). The peaks that emerge are described as typical peaks of the layered structure. The diffraction peaks of Ni/Al-Hc composite materials were in accordance with JCPDS No. 15-0087 with diffraction of 2  $\theta$  10.9°(003), 34.5°(012), and 61.6°(110). The

diffraction peaks of the Cu/Al-Hc composite material shown in Figure 1(d) have diffraction peaks at 12.75°(003), 18.9°(002), 36.44°(012), and 61.5°(110) was identified as a layered structure according to JCPDS No.30-0630. Figure 1(e) shows the Zn/Al-Hc difactogram with peaks at 2  $\theta$  angles around 9.78°(003), 19.66°(002), 33.80°(012), and 60.24°(110) according to JCPDS No. 48.2023. In

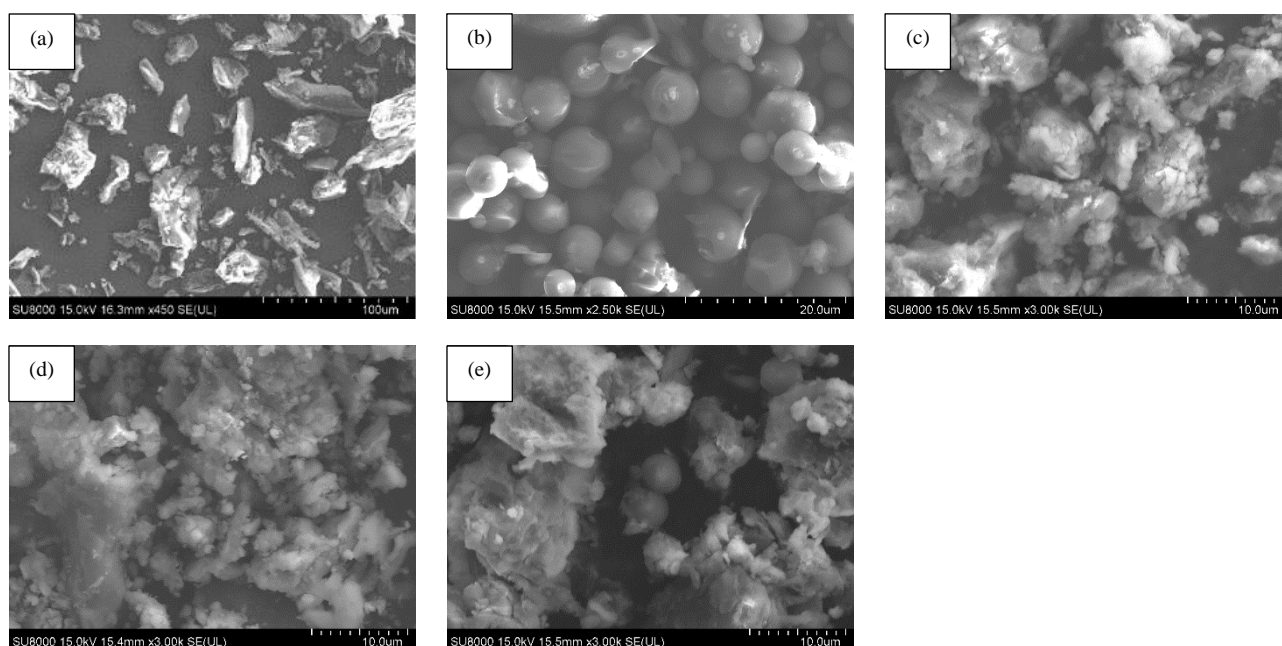
addition, [Figure 1](#) shows a typical diffraction peak of Hc around  $19^\circ$  to  $22.9^\circ$  with a reflection plane (002) identified as a cellulose compound from rambutan peel. Based on the results of the analysis, the preparation of composite materials in the form of Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc has been successfully prepared as evidenced by the appearance of diffraction peaks for pure LDH and Hc as the base material.

The successful preparation of the LDH-Hc composite material is supported by the FT-IR characterization presented in [Figure 2](#). The spectra of the Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc composites have the characteristics of pure LDH and Hc, which appear about  $3,424\text{ cm}^{-1}$  which corresponds to the vibration of the -OH group on the surface of the LDH layer, the peak of  $1,635\text{ cm}^{-1}$  indicates the vibration of water molecules between the LDH layer, the vibration at the peak of about  $<1,000\text{ cm}^{-1}$  indicates the presence of metal molecules bound to oxygen in the LDH layer. LDHs (M-O, M-O-M, O-M-O) are characteristics of LDH ([Hu et al., 2019](#)). In addition, the vibrations that appear in  $2953\text{ cm}^{-1}$  are associated with the C-H group, the  $1,683\text{ cm}^{-1}$  peak associated with the C-O group and the  $1,013\text{ cm}^{-1}$  peak associated with the C=C group which is characteristic of cellulose compounds in Hc materials ([Castro and das Virgens, 2019](#)). The LDH-Hc composite material has a vibration similar to that of pure LDH and Hc. FT-IR data confirm the successful modification of LDH with Hc.



**Figure 2.** Spectrum FT-IR of Rambutan peel (a), Hc (b), Ni/Al-Hc (c), Cu/Al-Hc (d), and Zn/Al-Hc (e)

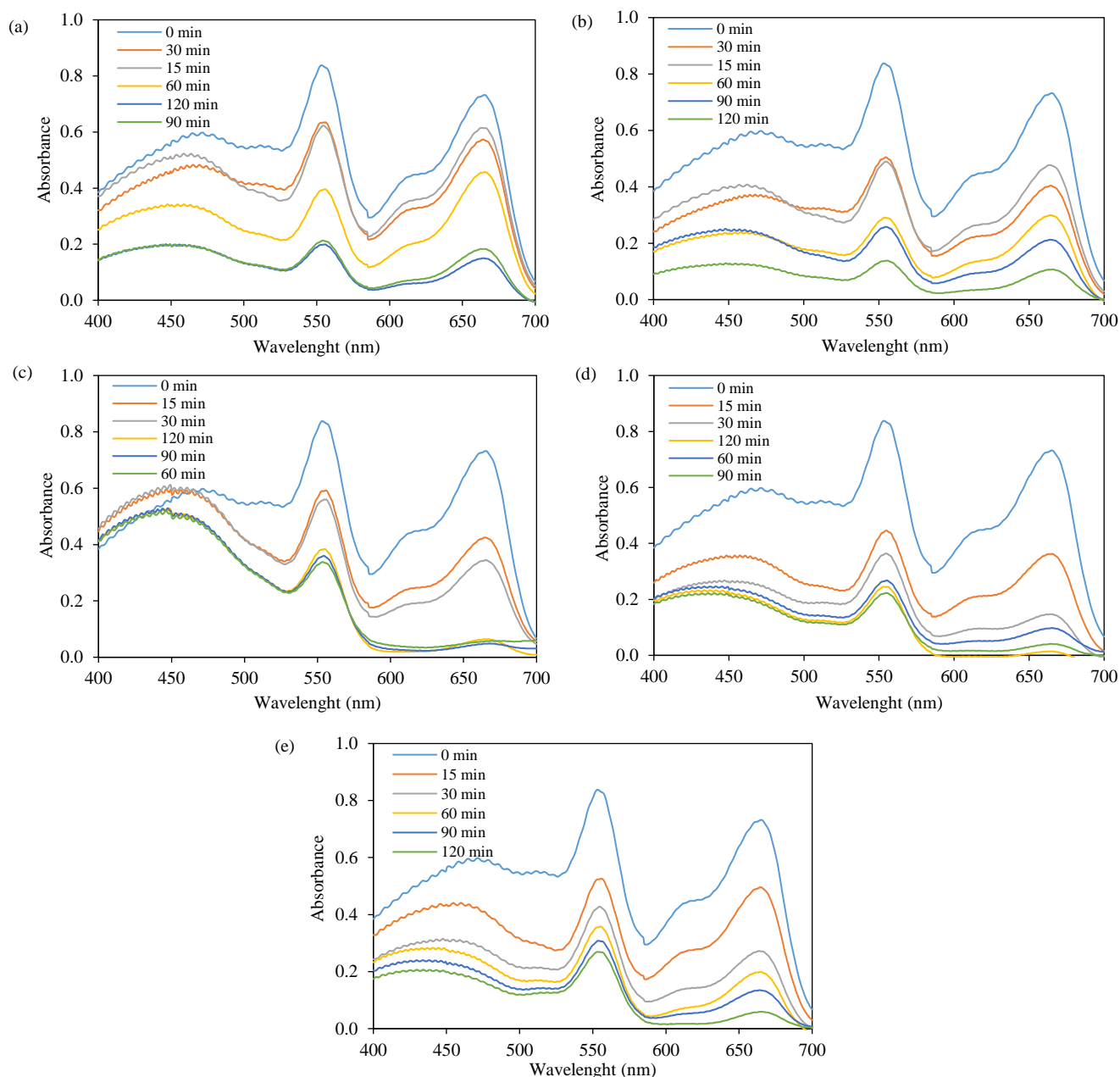
SEM analysis is used to see the surface morphology of the material. The results of the SEM analysis of the material are presented in [Figure 3](#). The rambutan peel shown in [Figure 3\(a\)](#) has a surface morphology with flat-shaped particles but heterogeneous in size and rough surface texture, while the Hc shown in [Figure 3\(b\)](#) has a surface morphology with particles shaped like round like a ball and more homogeneous in size. This is caused by the degradation of lignin and cellulose compounds in rambutan peels during the carbonization process. LDH-Hc in the form of Ni/Al-Hc (c), Cu/Al-Hc (d) and Zn/Al-Hc (e) has a rough, uneven surface texture and irregular pores and has a pore size of large pores with high aggregates.



**Figure 3.** SEM image of Rambutan peel (a), Hc (b), Ni/Al-Hc (c), Cu/Al-Hc (d), and Zn/Al-Hc (e)

The adsorption selectivity was carried out by mixing four dyes in the form of methylene blue (MB), rhodamine-B (Rh-B), methyl red (MR), and methyl orange (MO) with a concentration of 8 mg/L added to each of the peel adsorbents. rambutan, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc, and the wavelength at the maximum absorbance of the mixed dye solution was measured using a UV-Vis spectrophotometer. The results of these measurements are presented in Figure 4. The adsorption selectivity of the mixed dye was analyzed from changes in the adsorbed concentration which progressively increased during the adsorption process from 0, 15, 30, 60, to 120 min. Figure 4 shows the results of the adsorption selectivity on MB dye at first 8.33 mg/g, rambutan peel to 4.11 mg/g, Hc to

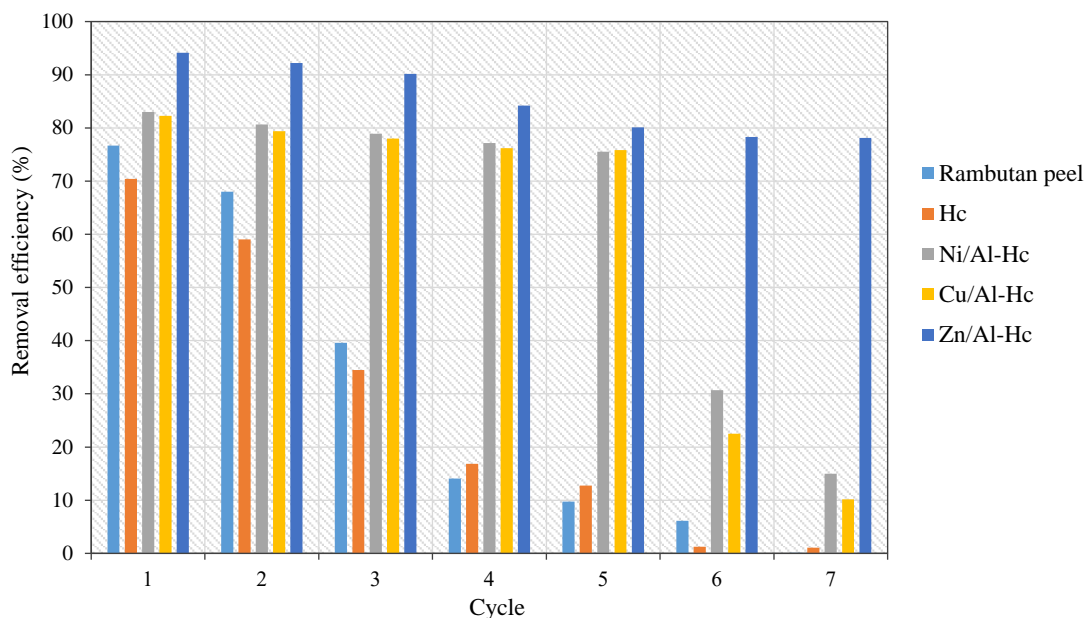
2.56 mg/g, Ni/Al-Hc to 0.2 mg/g, Cu/Al-Hc to 1.68 mg/g, and Zn/Al-Hc to 0.26 mg/g. Rh-B dye was initially 8.26 mg/g, rambutan peel was 6.01 mg/g, Hc to 2.45 mg/g, Ni/Al-Hc to 1.04 mg/g, Cu/Al-Hc to 3.98 mg/g, Zn/Al-Hc to 0.71 mg/g, for MR dyes initially at first of 8.13 mg/g, rambutan peel of 6.01 mg/g, Hc to 6.53 mg/g, Ni/Al-Hc to 2.64 mg/g, Cu/Al-Hc to 5.13 mg/g, and Zn/Al-Hc to 2.8 mg/g. MO at first was 8.24 mg/g, rambutan peel was 8.18 mg/g, Hc to 5.87 mg/g, Ni/Al-Hc to 3.49 mg/g, Cu/Al-Hc to 4.12 mg/g, and Zn/Al-Hc to 3.83 mg/g. A drastic decrease occurred at minute 120 with each adsorbent adsorbent. It can be concluded that the dye is selective for the adsorbent of rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc are MB dye. After knowing



**Figure 4.** UV-Visible spectra of mixture MB, Rh-B, MR, and MO on Rambutan peel (a), Hc (b), Ni/Al-Hc (c), Cu/Al-Hc (d), and Zn/Al-Hc (e)

the most selective dye was MB, then MB was continued for the adsorption process using regeneration studies and adsorption isotherms and thermodynamic adsorption processes to determine the effectiveness of the adsorbent in removing MB.

Furthermore, conducting a regeneration study to determine the effectiveness of each adsorbent for repeated use. The results of the study regeneration of rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc are shown in Figure 5.



**Figure 5.** Rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc adsorbent regeneration ability

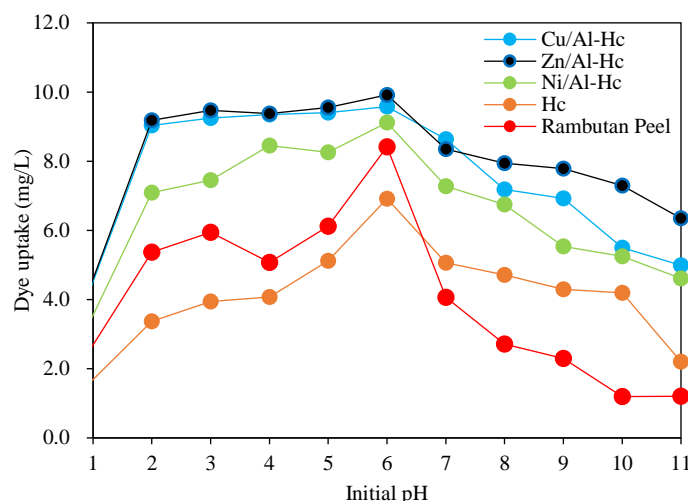
Rambutan peel, Hc, Ni/Al-Hc, and Cu/Al-Hc composites showed a decrease in adsorption ability. Rambutan peel had an adsorption capacity of 76.65% in the first cycle and decreased to 0.12% in the last cycle. Hc has a cycle I of 70.43%, and its ability also decreased to 1.09% in the last cycle. The results of the regeneration of Zn/Al-Hc composites showed a stable adsorption ability compared to Ni/Al-Hc and Cu/Al-Hc. Ni/Al-Hc reached 83.02% in the first cycle and decreased to 14.98% for the last cycle, while Cu/Al-Hc in the first cycle was 82.29% and the last cycle decreased to 10.13%. Zn/Al-Hc reached the first cycle of 94.13%, the second was 92.19%, the third was 90.13%, the fourth was 84.21%, the fifth was 80.12%, the sixth was 78.33% and the last one was 78.11%. Rambutan peel, Hc, Ni/Al-Hc, and Cu/Al-Hc experienced a very significant decrease while the Zn/Al-Hc composite material decreased but not significantly. Based on these data, Zn/Al-Hc has the best regeneration ability compared to rambutan peel, Hc, Ni/Al-Hc, and Cu/Al-Hc.

The variation of pH adsorption of methylene blue using rambutan peel adsorbents, Hc, Ni/Al-Hc, and Cu/Al-Hc is shown in Figure 6.

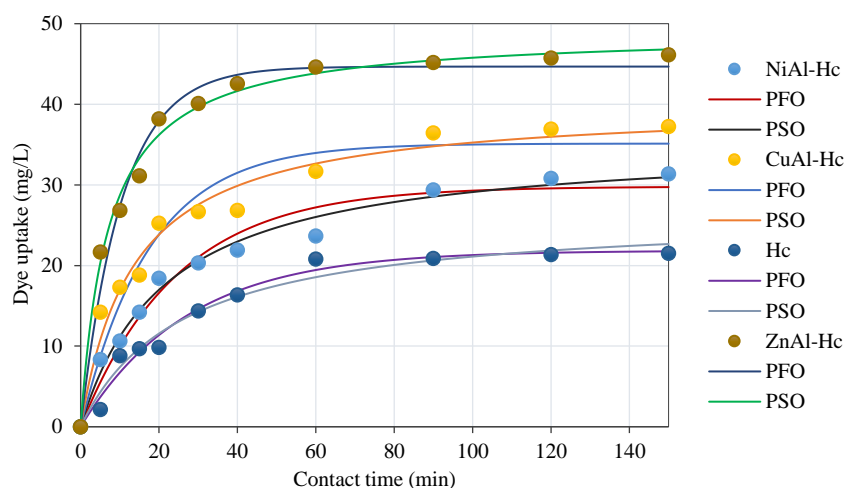
On rambutan peel Hc, Ni/Al-Hc, Cu/Al-Hc, and

Zn/Al-Hc the maximum adsorption of MB occurred at the optimum pH which was pH 6. Experiments with pH variations were generally carried out to determine the optimum pH for MB adsorption. Based on Mantasha et al. (2020), the OH<sup>-</sup> ion from the adsorbent at acidic pH of blue will maintain the N group in the methylene dye, so that the interaction between methylene blue and the adsorbent will increase and the attractive force that occurs is also getting bigger. Meanwhile, at alkaline pH, methylene blue forms a salt that ionizes the negatively charged Cl<sup>-</sup> group and at the same time OH<sup>-</sup> ions from the adsorbent will inhibit the absorption process caused by the formation of repulsion by the same charge around the surface of the adsorbent with a charge of methylene blue dye. Which causes the methylene blue dye to be difficult to apply to the adsorbent surface.

The adsorption ability on the adsorption kinetics parameters can be seen in Figure 7. Find the adsorption kinetics model using Equations 1 and 2 in the form of Pseudo First Order (PFO) and Pseudo Second Order (PSO) equations. Adsorbents Hc, Ni/Al-Hc, Cu/Al-Hc and Zn/Al-Hc composites on the MB adsorption kinetics process showed that the absorption time occurred at 100 min. The parameters calculated from Equations 1 and 2 are shown in Table 1.



**Figure 6.** The effect of pH on adsorption capacity of adsorbent (rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, Zn/Al-Hc) and removal of MB



**Figure 7.** Adsorption kinetics model of MB using Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc

**Table 1.** Kinetic parameters of dyes adsorption onto Hc, Zn/Al-Hc, Cu/Al-Hc, and Ni/Al-Hc

Adsorbent	$Q_{e\text{experiment}}$ (mg/g)	PFO			PSO		
		$Q_{e\text{Calc}}$ (mg/g)	$R^2$	$k_1$	$Q_{e\text{Calc}}$ (mg/g)	$R^2$	$k_2$
Hc	46.143	24.400	0.938	0.037	47.619	0.998	0.097
Zn/Al-Hc	44.705	41.763	0.974	0.038	49.261	0.995	0.007
Cu/Al-Hc	31.381	29.356	0.970	0.030	35.971	0.993	0.022
Ni/Al-Hc	21.450	24.160	0.965	0.047	27.173	0.952	0.016

One of the most important characteristics in the adsorption process is kinetics. To clarify the adsorption kinetics of MB using the Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc composites adsorbent, the kinetic models, PFO and PSO were used. For the study of adsorption kinetics, the concentration of MB used was 50 mg/L with varying times ranging from 0 to 180 min and 0.02 g of adsorbent was added at the optimum condition of pH 6. The PSO model as the equation was assumed to be ideal on the adsorption

surface of MB. The constant values of  $K_1$  and  $q_e$  were calculated from the slope and intercept  $\log (q_e - q_t)$  versus  $t$  (Equations 1-2).

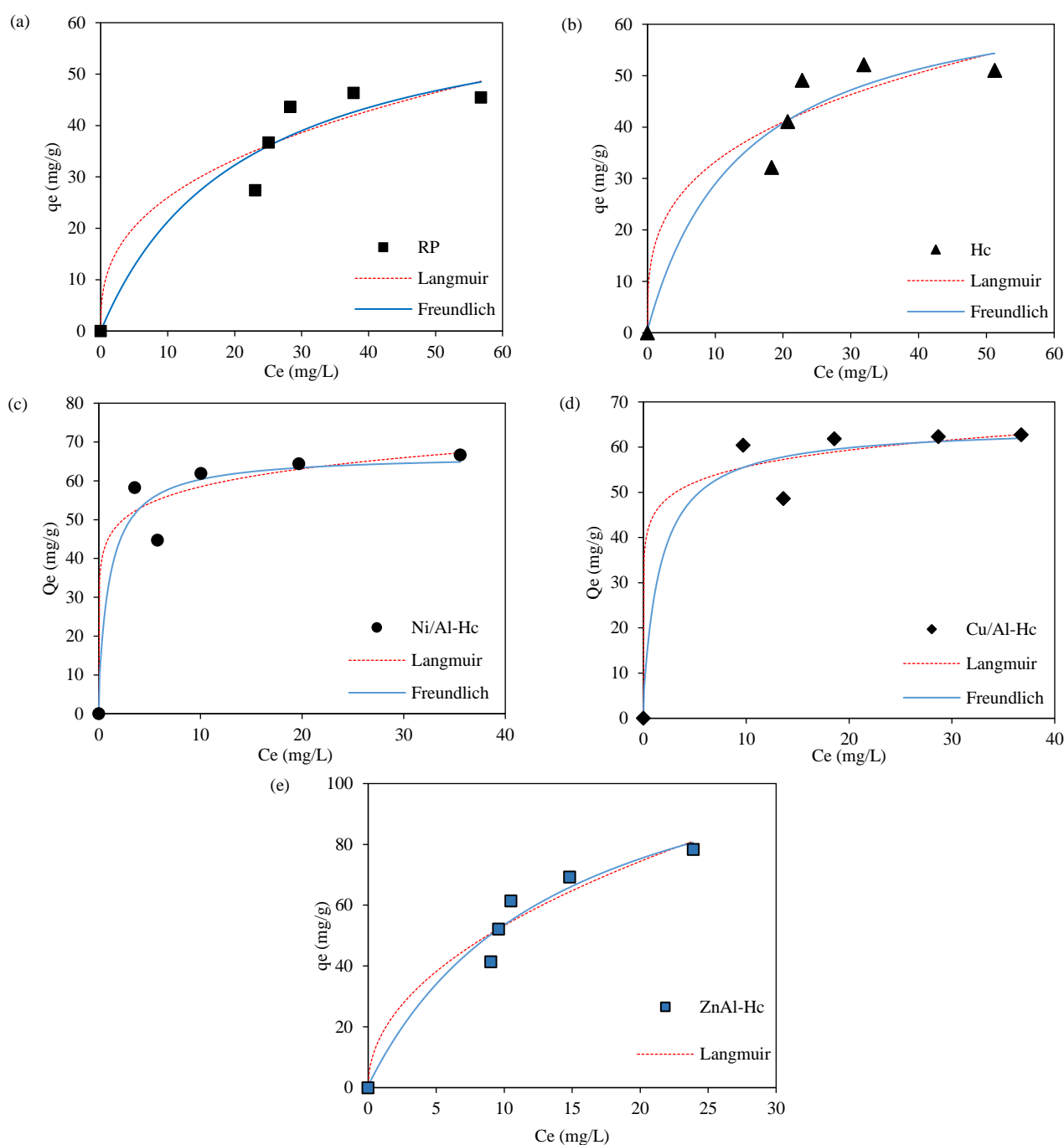
Table 1 shows that the adsorption kinetics tend to follow the PSO model with a linear regression value that is closer to 1 ( $R^2 > 0.952$ ). Each adsorbent reached the optimal  $q_e$  value with the adsorption equilibrium time at 100 minutes. The largest value of  $q_e$  It can be seen that the PSO model is almost right for the first step. However, the PSO kinetic model seen from the

highest linear regression  $R^2$  (Table 1) and seen from the adsorption capacity value calculated from the pseudo model is close to the experimental value, which shows that the dominant kinetic phenomenon of PSO for MB adsorption by the adsorbent Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc composites with the dominant adsorption process occurring chemical interactions between the adsorbent and the adsorbate.

Furthermore, the adsorption ability is determined through the isotherm parameters which can be presented in Figure 8. Determination of the adsorption isotherm is determined through the

Langmuir and Freundlich equations based on Equations 3 and 4.

Figure 8 shows the Langmuir and Freundlich isotherm model pattern. Figure 8 shows that the Zn/Al-Hc composite material has a higher adsorbed concentration ( $q_e$ ) than rambutan peel, Hc, Ni/Al-Hc, and Cu/Al-Hc. Figure 6 on rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc looks lower for MB adsorption. Determination of the adsorption isotherm model through the linear regression value of  $R^2$  which is close to 1. The calculated data are presented in Table 2.



**Figure 8.** Adsorption isotherm model of MB using Rambutan peel (a), Hc (b), Ni/Al-Hc (c), Cu/Al-Hc (d), and Zn/Al-Hc (e)

Table 2 shows the Langmuir and Freundlich isotherm data in the form of Langmuir constant ( $k_L$ ), maximum adsorption capacity ( $q_m$ ), adsorption intensity ( $n$ ), and Freundlich constant ( $k_F$ ). Table 1 shows the Langmuir data at the Langmuir constant value ( $k_L$ ) of 0.070, 0.080, 0.025, 0.074, 0.040 and is in the range of 0 and 1 which identifies a suitable system for the adsorption process (Mishra et al., 2020; Zhao et al., 2020). The  $q_m$  data shows the value of large adsorption capacity on the adsorbent of LDH-Hc composite materials (Ni/Al-Hc, Cu/Al-Hc, Zn/Al-Hc) reaching 144.928 mg/g, 175.439 mg/g, 217.910 mg/g while rambutan peel precursors and Hc had lower adsorption capacities of 43.860 mg/g and 49.286 mg/g, respectively. Furthermore, Table 2 is equipped with data on the Freundlich isotherm with the value of

the Freundlich constant ( $k_F$ ) and the value of  $n$  where the  $k_F$  value reaches 0.921 to 20.029 which is related to the binding energy between the adsorbate and the adsorbent, while the adsorption intensity ( $n$ ) with a value of  $n$  reaches 0.285 to 10.560 related according to the adsorption process.

Based on Table 2, the adsorption process tends to follow the Freundlich isotherm according to the linear coefficient value ( $R^2$ ) which is closer to 1. Freundlich isotherm is an adsorption process following adsorption by multilayer adsorption and Freundlich can also describe physical adsorption (Wang et al., 2020) is supported by a value of  $1/n < 1$  (Table 2) as the intensity of multilayer adsorption of adsorbate molecules on the surface of a heterogeneous material (Binh and Nguyen, 2020).

**Table 2.** Isotherm model of MB adsorption on Rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc

Materials	Langmuir			Freundlich		
	$q_m$ (mg/g)	$k_L$	$R^2$	$n$	$k_F$	$R^2$
Rambutan peel	43.860	0.070	0.995	0.285	20.029	0.999
Hc	49.286	0.080	0.999	4.651	4.870	0.999
Ni/Al-Hc	144.928	0.025	0.991	2.699	10.737	0.999
Cu/Al-Hc	175.439	0.074	0.936	10.560	0.921	0.999
Zn/Al-Hc	217.391	0.040	0.989	1.863	15.153	0.994

The comparison of MB adsorption for several adsorbents is presented in Table 3. Table 3 shows the adsorption capacity of several adsorbents for MB dye. Comparison between the performance of the adsorbent and various adsorbents that have a value ( $q_m$ ) which is associated with the maximum adsorption capacity of the adsorbent for the removal of the adsorbent in the form of MB. It can be seen that Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc have a larger adsorption capacity in MB removal, this is due to the large surface area and more active sites of LDH and Hc. so that the interaction of the adsorbate with the adsorbent is more so that the adsorption capacity is large. The adsorbents prepared in this study have higher adsorption capacities when compared with the ones on Table 3.

Furthermore, the thermodynamic parameters provide data on the Gibbs free energy ( $\Delta G$ ), enthalpy ( $\Delta H$ ), and entropy ( $\Delta S$ ) which are calculated according

to Equations 3 and 4. The adsorption thermodynamic data are shown in Table 4.

Table 4 shows the results of the calculation of negative adsorption values for  $\Delta G$  on each adsorbent.  $\Delta G$  values increase with increasing adsorption temperature from 30°C to 60°C. A negative value  $\Delta G$  indicates that the MB adsorption process takes place spontaneously (Normah et al., 2021b). In this study, the  $\Delta H$  value showed a range of 10.851 kJ/mol to 42.150 kJ/mol which was related to the tendency of MB adsorption to occur by physical adsorption and a positive  $\Delta H$  value indicated that MB adsorption was endothermic (Wijaya et al., 2021). The value of  $S^\circ$  is positive and is in the range of 0.037 J/mol·K to 0.144 J/mol·K. This is related to the irregularity of the particles during the adsorption process which increases due to the interaction between solid in the form of adsorbent-liquid in the form of MB adsorbate.

**Table 3.** Comparison of several adsorbents to removal MB

Adsorbent	Adsorption capacity (mg/g)	Reference
Cellulosic olice stones biomass	22.4	Al-Ghouti and Al-Absi (2020)
Fe <sub>3</sub> O <sub>4</sub> @C <sub>60</sub> @MA	7.51	Xu et al. (2020)
Scenedesmus microalgae	55.26	Rathee et al. (2019)

**Table 3.** Comparison of several adsorbents to removal MB (cont.)

Adsorbent	Adsorption capacity (mg/g)	Reference
Bio-adsorbent of <i>Pleurotus eryngii</i>	18.45	<a href="#">Wu et al. (2019)</a>
PDOPA-f-Mg/Al LDH	132	<a href="#">Zhao et al. (2017)</a>
MnMgFe	20	<a href="#">Khuluk et al. (2019)</a>
Ni/Fe/Ti LDH	29.940	<a href="#">Rathee et al. (2019)</a>
Mg3AlDBS	10.864	<a href="#">Abdellaoui et al. (2019)</a>
Rambutan peel	57.803	In this study
Hc	49.286	In this study
Ni/Al-Hc	144.928	In this study
Cu/Al-Hc	175.439	In this study
Zn/Al-Hc	217.391	In this study

**Table 4.** Thermodynamic parameters of MB adsorption on Rambutan peel, Hc, Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc

Parameters	T (K)	Materials				
		Rambutan peel	Hc	Ni/Al-Hc	Cu/Al-Hc	Zn/Al-Hc
$\Delta G$	303	-0.210	-0.430	-1.479	-0.368	-1.373
	313	-0.566	-0.956	-2.076	-0.739	-2.809
	323	-1.011	-1.481	-2.672	-1.109	-4.246
	333	-1.807	-2.007	-3.269	-1.479	-5.682
$\Delta S$		0.053	0.053	0.060	0.037	0.144
$\Delta H$		15.503	15.503	16.593	10.851	42.150

#### 4. CONCLUSION

In this study, LDH in the form of Ni/Al, Cu/Al, and Zn/Al were synthesized using the coprecipitation method and modified with hydrochar from rambutan peel which was prepared using the hydrothermal carbonization method. The material was applied as an adsorbent for the removal of methylene blue in aqueous solution using UV-Vis spectrophotometric method. The manufacture of LDH-Hc composites was proven by XRD, FT-IR, and SEM analysis. The results of adsorption selectivity showed that LDH with rambutan peel hydrochar showed good selective ability for methylene blue and regeneration studies showed that the LDH-Hc composite showed a more stable adsorption regeneration ability reaching seven regeneration cycles for Zn/Al-Hc, while Ni/Al-Hc and Cu/Al-Hc achieved five regeneration cycles compared to LDH without modification, which only achieved three regeneration cycles using water solvent. The optimum pH of MB was found at pH 6. The study of adsorption kinetics was carried out using pseudo first order and pseudo second order equations and the removal of conformity MB followed the pseudo second order kinetic model. Parameter data of concentration and temperature of adsorption using Langmuir and Freundlich equation was determined. The results showed that the adsorption matched the

Freundlich isotherm model with adsorption capacity ( $q_m$ ) using Ni/Al-Hc, Cu/Al-Hc, and Zn/Al-Hc adsorbents reaching 144.928, 175.439, and 217.391 mg/g, respectively, with the adsorption process taking place continuously, spontaneously, and endothermically. The performance of the LDH-Hc composite using the adsorption method is superior to many other materials that have been used for dye absorption in the literature.

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